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# ADSORPTIVE INTERACTIONS BETWEEN MEMBRANES AND TRACE CONTAMINANTS

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**ABSTRACT:** Widespread occurrences of endocrine-disrupting chemicals (EDCs) in waterways have attracted a great attention of the scientific community. While scientific evidence associated with human health is restricted due to the long-term effects, impacts of EDCs on trout at the common concentration encountered in sewage effluent have been confirmed by both in vitro and in vivo studies. The impacts of steroid estrogens such as estrone, estradiol (natural hormones) and ethinylestradiol (a synthetic hormone) are often more serious than other synthetic EDCs as they have far higher endocrine-disrupting potency, despite of their low concentration.

This paper investigates retention and adsorptive behavior of the natural hormones estrone by two commercial reverse osmosis membranes TFC-S and X-20, using dead end stirred cell systems. While an adsorptive process that reaches a breakthrough governs the retention of estrone by the TFC-S membrane; a sieving mechanism is responsible for the high removal of estrone using the X-20 membrane.

## Keywords

Endocrine disrupters, hormones, nanofiltration, adsorption, water and wastewater treatment.

## 1. INTRODUCTION

In vitro and in vivo studies by many researchers have confirmed the impacts of endocrine-disrupting chemicals (EDCs) on trout at the common concentration encountered in sewage effluent. Amongst many types of EDCs the impacts of steroid estrogens such as estrone, estradiol (natural hormones) and ethinylestradiol (a synthetic hormone) are prominent as they have far higher endocrine-disrupting potency than other synthetic EDCs (Johnson and Stumpter, 2001; Ternes et al., 1999a and 1999b). In spite of the magnitude of this problem, research on the removal of EDCs in water and wastewater treatment remains to date very limited due to their relatively low concentration and the associated analytical difficulties.

Advanced treatment technologies are required for more stringent requirements in water and wastewater treatment. Membrane processes have been widely accepted of being able to comply with such standards. As performance of conventional wastewater treatment of different plants on removal of steroid estrogens varies greatly and, concentrations of some steroid estrogens in secondary effluent are still able enough to harm wildlife such as fish in

particular (Johnson and Stumpter, 2001), reverse osmosis process is likely to play an important role in removal of these compounds. Retention of organic compounds by reverse osmosis membranes has been the subject of considerable research. Molecular weight of organic solutes and salt retention of the membranes may be a poor predictor of the retention (Wiesner and Buckley, 1996; Schaefer et al, 2001). Indeed, retention of organic solutes by RO membranes can be governed by a complex fashion on the chemistry of the solute-membrane interactions. Solute and solvent transport across the membrane can often be described in term of their affinity to the membrane material and their diffusive transport within the membrane. It has been observed that compounds that are capable of significant hydrogen bonding tend to be removed to a lesser extent (Wiesner and Buckley, 1996).

Several researchers have shown that nanofiltration and reverse osmosis processes is capable of removing trace organics including natural hormones and a wide range of pesticides (Kiso et al, 2001; Schäfer et al, 2001; Kiso et al, 2000). In our previous work, removal of the trace contaminant estrone using eight different nanofiltration and reverse osmosis membranes, which cover a wide pore size range, has been studied. It was found that estrone could be adsorbed to the surface of some membranes and subsequently give the impression of high retention. This adsorptive phenomenon is of concern as it may result in contaminants leakage or bulk release when desorption occurs. This paper investigates retention and adsorptive behavior of the natural hormones estrone on two RO membranes TFC-S and X-20.

## 2. MATERIALS AND METHODS

### 2.1 Membranes

Two reverse osmosis membranes TFC-S and X-20 were selected for this study due to their excellent salt retention of more than 99% as specified by the manufacturers. The former was supplied by Fluid System (San Diego, USA) and the latter was supplied by Trisep Corporation (Goleta, USA). Membrane material and pure water flux at 5 bar are summarised in Table 1. Assuming that the active layer thickness is the same, TFC-S is expected to have a larger pore size as compared to X-20 due to its higher pure water flux.

**Table 1:** Membrane types and pure water flux

Membrane Type	Average Pure Water Flux* [ $\text{Lm}^{-2}\text{h}^{-1}$ ]	Membrane resistance [ $\text{m}^{-1}$ ]	Membrane material
TFC-S	$55.0 \pm 7.3$	$3.3 \cdot 10^{13}$	Polyamide on Polysulfon support
X-20	$20.5 \pm 2.4$	$8.8 \cdot 10^{13}$	Polyamide-urea Composite

\* Average values are derived from all experiments and variations are averaged.

### 2.2 Filtration System and Protocol

Experiments were carried out in a 185 mL stainless steel stirred cell. Details of the filtration system were described elsewhere (Nghiem et al., (accepted)). The inner diameter was 56.6 mm resulting in a membrane surface area of  $21.2 \text{ cm}^2$ . An Amicon magnetic stirrer was used and the stirrer speed was set at 400 rpm to minimize polarization concentration effects. Instrument grade air was used to pressurize the stirred cell. A new membrane was used for each experiment.

Each experiment was conducted in three steps. The membrane was compacted for 1 hour using MilliQ water at 10 bar. Pure water flux was then determined at 5 bar. In the third step, the reservoir was emptied and the cell filled with the test solution. The solution was filtered at 5 bar or 10 bar for TFC-S and X-20 membranes respectively, to obtain

compatible flux. Six permeate samples of 20 mL each were collected from the filtration of a feed volume of 185 mL. A retentate sample was also collected for analysis.

### 2.3 Solution Chemistry and Chemicals

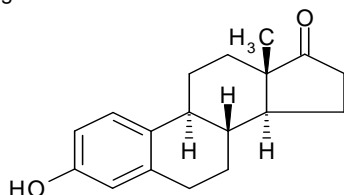
All chemicals were of analytical grade. Radiolabelled estrone-2,4,6,7-<sup>3</sup>H(N) was purchased from Sigma Aldrich (Saint Louis, Missouri, USA). The background electrolyte consisted of 1 mM NaHCO<sub>3</sub>, and 20 mM NaCl. pH was adjusted using 1M HCl or 1M NaOH.

### 2.4 Natural Hormone Characteristics and Analysis

Molecular structure of estrone is presented in Figure 2. Being hydrophobic, estrone has a very low solubility in water (Merck, 1996). Diameter of the molecule is estimated to be about 0.8 nm using Stokes-Einstein equation. The acid dissociation constant, pKa, of estrone is 10.4 (Schäfer et al., (submitted)). Hydroxyl and carbonyl functional groups of estrone can facilitate the formation of hydrogen bonding between the molecule and the membrane surface. Theoretically, estrone can be either a proton-donor or a proton-acceptor species.

Feed solution was prepared by spiking estrone into background electrolyte solution to a estrone concentration of 100 ng/L, which presents a typical concentration of natural hormones often encountered in water and wastewater treatment.

Estrone was analysed using a Packard Instruments scintillation counter.



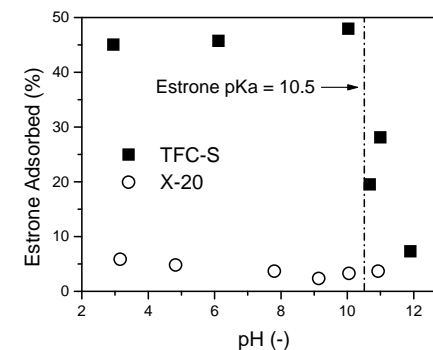
**Figure 1:** Molecular structure of estrone.

Adsorption of estrone to the membrane was determined by cutting the membrane into small pieces at the conclusion of each experiment. The membrane was then placed into a scintillation vial to which 5 mL of acetone was added. The vial was shaken vigorously and left for 1 hour for all estrone to dissolve. 1 mL of solution was extracted into another vial for air dry. This was redissolved with 1 mL of MilliQ water and added with 9 mL of scintillation liquid prior to analysis. Adsorption was also determined using mass balance and both methods produced similar results.

## 3. RESULTS AND DISCUSSION

### 3.1 Solute-membrane interactions

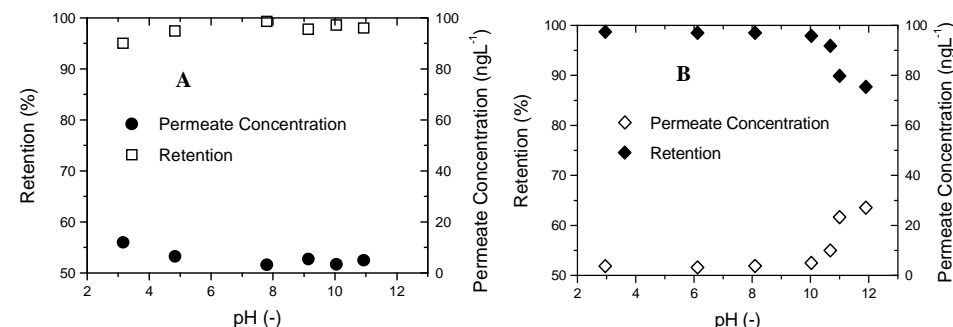
Figure 2 shows that adsorption of estrone by TFC-S membrane drops drastically with the dissociation of estrone at pH 10.5. Unfortunately, the experiments do not allow differentiation between adsorption on the active layer and the support material. Hydrogen bonding was suggested as the mechanism of adsorption of estrone by the membrane (Schäfer et al., (submitted)). Hydroxyl groups are the most likely interaction sites due to the resonance structures of the aromatic groups. When dissociated, estrone loses its proton and becomes unable to participate in hydrogen bonding with membrane functional groups, resulting in a reduction in adsorption and lower retention. Surprisingly, adsorption of estrone by X-20 is low and remains unchanged regardless the pH of the matrix solution, despite the fact that the membrane is also made of polyamide.



**Figure 2:** Estrone adsorption as a function of pH on TFC-S and X-20 membranes (100 ng/L estrone; 1 mM NaHCO<sub>3</sub>; 20 mM NaCl).

### 3.2 Estrone retention

Figure 3 compares estrone retention and concentration of permeates following membrane filtration by TFC-S and by X-20 at different pH. Retention by the TFC-S membrane decreases by about 10% as pH exceeds pKa value of estrone (10.5) in parallel with the decreased adsorption, which was presented in Figure 2. In contrast, the estrone adsorption by the X-20 membrane is unchanged and subsequently retention is unaffected by the pH of the matrix solution.



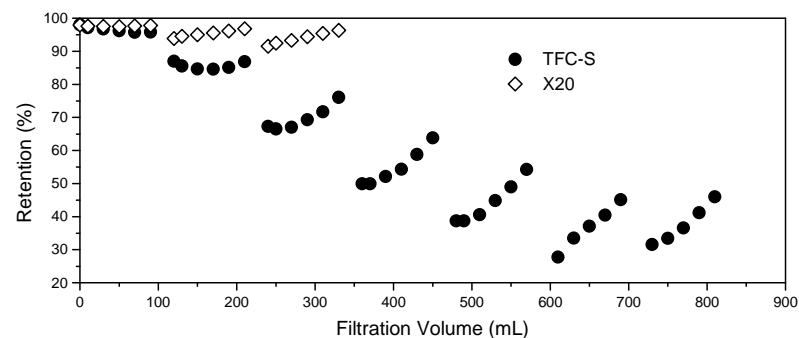
**Figure 3:** Permeate concentration and estrone retention by X-20 (A) and TFC-S (B) membranes as function of pH (100 ng/L estrone; 1 mM NaHCO<sub>3</sub> and 20 mM NaCl)

Mass transport of the solute across a RO membrane may involve in three major consecutive steps: (1) diffusion from the water phase into the pore of the membrane; (2) sorption onto then diffusion across the membrane; (3) desorption from the permeate side of the membrane (Chen et al., 2001). It is estimated that the molecular size of estrone is in the same order of magnitude as the pore size of the TFC-S membrane (approximately 0.8 nm in diameter), while water molecules are much smaller. Transport of estrone across this membrane depends on the rate of adsorption (the formation of hydrogen bonding). Since estrone adsorption involves a more specific chemical interaction, estrone is tightly bound

to specific sites and much less mobile than in physical adsorption. Estrone molecules are instead believed to 'hop' from one site to the next when subjected to the chemical potential across the membrane. As a result, estrone transport is retarded across the membrane layer and consequently estrone retention depends on the adsorption process. This then becomes apparent in a breakthrough curve.

It is speculated that the pore size of the X-20 membrane is smaller than estrone molecule; thus, diffusion of estrone from the water phase into the membrane pore is not favorable. Diffusion controls the rate of estrone transfer across the membrane and sieving mechanism is mainly responsible for the separation process.

### 3.3 Long term performance



**Figure 4:** Retention as a function of filtration volume (100 ng/L estrone; 1 mM NaHCO<sub>3</sub>, 20 mM NaCl and pH 7.8).

It appears that adsorption of trace contaminants on membranes is a temporary effect that occurs in the initial stages of filtration. While this adsorption should not be relied upon for the removal of trace contaminants, adsorption is likely to continue until the material is saturated and lead to the accumulation of large amounts of contaminants (Nghiem et al., (accepted)).

To investigate the limits of this adsorption and subsequent retention of saturated membranes, experiments were conducted with a series of fresh feed solutions for one membrane. Results from these experiments are presented in Figure 4. This indicates that the adsorption is reversible and it only slows down estrone flux across the membrane temporarily.

Not surprisingly, estrone retention by X-20 membrane remains almost unchanged after three fresh feed solutions were filtered. A negligible reduction in retention was probably due to the operation mode of the dead end stirred cell where bulk concentration suddenly changed in the transition of a fresh feed solution to the next.

### 4. CONCLUSIONS

In this study, we investigated the adsorptive phenomena of natural hormones estrone by two RO membranes. pH has been found to influence the adsorption of estrone by TFC-S

membranes, presumably due to hydrogen bonding, while the estrone adsorption by the X-20 membrane remains unchanged. Chemical interactions between estrone and the TFC-S membrane control the rate of mass transfer of the solute across the membrane. Retention is very low when the membrane is saturated. Steric exclusion appears to be the major mechanism contributing to the removal of estrone in aqueous solution for X-20 membrane.

### 5. ACKNOWLEDGEMENTS

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